

AMENDMENTS TO THE CLAIMS

1. (Currently amended): A process for demineralizing coal comprising:
 - (a) forming a slurry of coal particles in an alkali solution;
 - (b) maintaining the slurry at a temperature of 150-250 °C under a pressure sufficient to prevent boiling;
 - (c) separating the slurry into an alkalized coal and a spent alkali leachant;
 - (d) forming an acidified slurry of the alkalized coal, said acidified slurry having a pH of 0.5-1.5;
 - (e) separating the acidified slurry into a coal-containing fraction and a substantially liquid fraction;
 - (f) subjecting the coal-containing fraction to a hydrothermal washing step to remove Si, Fe and/or Ti from the coal comprising:
 - (1) mixing the coal-containing fraction with water and (a) a polar organic solvent or (b) citric acid to form a mixture, and
 - (2) heating the mixture to a temperature of from 150 °C to 280 °C under a pressure sufficient to prevent boiling; and
 - (g) separating the ~~coal from the~~ mixture in of step (f) into a liquid portion containing Si, Fe and/or Ti and a coal containing portion.
2. (Original): A process as claimed in claim 1 wherein the coal provided to step (a) is sized such that 100% is less than 1mm.
3. (Original): A process as claimed in claim 2 wherein the coal provided to step (a) is sized such that 100% less than 0.5mm.

4. (Previously presented): A process as claimed in claim 2 wherein the coal provided to step (a) contains 5% by weight smaller than 20 microns.

5. (Previously presented): A process as claimed in claim 1 wherein the slurry formed in step (a) has a coal concentration of from 10% to 30% by weight.

6. (Original): A process as claimed in claim 5 wherein the coal concentration in the slurry is about 25% by weight.

7. (Previously presented): A process as claimed in claim 1 wherein an alkali concentration in a liquid phase of the slurry is in the range of 8% to 20% by weight (calculated as NaOH equivalent).

8. (Original): A process as claimed in claim 7 wherein the alkali concentration is from 13% to 15% by weight (calculated as NaOH equivalent).

9. (Previously presented): A process as claimed in claim 1 wherein the slurry is heated to a temperature of from 220-250 °C in step (b).

10. (Previously presented): A process as claimed in claim 1 wherein the slurry is maintained at an elevated temperature in step (b) for a period of from 15 to 60 minutes.

11. (Previously presented): A process as claimed in claim 1 wherein a rate of heating the slurry is maintained at a rate of less than 2°C per minute in the temperature range of 150 °C to 250 °C.

12. (Previously presented): A process as claimed in claim 1 wherein the slurry in step (b) is maintained at the autogenous pressure of the heated slurry to prevent the slurry from boiling.

13. (Previously presented): A process as claimed in claim 1 wherein step (c) takes place at a temperature of from 30 °C to 80 °C.

14. (Previously presented): A process as claimed in claim 13 wherein the slurry from step (b) is cooled to a temperature of from 30-80 °C at a cooling rate of less than 20°C/minute and at 2 °C per minute whilst the temperature of the slurry is in the range of 240 °C – 150 °C.

15. (Previously presented): A process as claimed in claim 1 wherein the alkalized coal recovered from step (c) is washed to remove excess alkali.

16. (Previously presented): A process as claimed in claim 1 wherein the alkalized coal from step (c) is treated to remove sodium aluminosilicates therefrom prior to sending to step (d).

17. (Previously presented): A process as claimed in claim 1 wherein step (d) comprises mixing the coal from step (c) with water or an acid solution to obtain a slurry having a coal concentration that falls within the range of 5% to 20% by weight.

18. (Original): A process as claimed in claim 17 wherein the slurry has a coal concentration of about 10% by weight.

19. (Previously presented): A process as claimed in claim 1 wherein the slurry in step (d) contains a mineral acid.

20. (Original): A process as claimed in claim 19 wherein the mineral acid is sulphuric acid or hydrochloric acid.

21. (Previously presented): A process as claimed in claim 1 wherein the slurry of step (d) has a pH that falls in the range of 0.5 to 1.5.

22. (Original): A process as claimed in claim 21 wherein the pH of the slurry is about 1.0.

23. (Previously presented): A process as claimed in claim 1 wherein the temperature of the slurry in step (d) falls within the range from 20 °C to 90 °C.

24. (Original): A process as claimed in claim 23 wherein the temperature falls within the range of from 30 °C to 60 °C.

25. (Previously presented): A process as claimed in claim 1 wherein the coal is maintained in contact with the acid solution in step (d) for a period of at least 1 minute.

26. (Original): A process as claimed in claim 25 wherein the coal is maintained in contact with the acid solution in step (d) for a period of about 60 minutes.

27. (Previously presented): A process as claimed in claim 1 wherein the coal fraction from step (e) is re-slurried with water and acid and brought to a pH of between 0.5 and 1.0 for a further period of time of greater than 1 minute.

28. (Original): A process as claimed in claim 27 wherein the step of re-slurrying the coal is repeated between one and four times.

29. (Previously presented): A process as claimed in claim 1 wherein step (f) comprises mixing the coal-containing fraction with a solution of water and a polar organic solvent that is an alcohol selected from ethanol, methanol, propanol or mixtures thereof.

30. (Previously presented): A process as claimed in claim 29 wherein the polar organic solvent is ethanol.

31. (Currently amended): A process as claimed in claim 1 wherein, ~~in the mixture of step (f)[[,]] the coal is mixed with~~ comprises water and a polar organic solvent such ~~that a slurry having and has~~ a solids content of 10-30% by weight ~~is formed~~.

32. (Currently amended): A process as claimed in claim 31 wherein the ~~slurry mixture in step (f)~~ has a pH of from 1.5 to 2.5.

33. (Currently amended): A process as claimed in claim 29 wherein the ~~slurry mixture in step (f)~~ is heated to a temperature of from 240 °C to 280 °C ~~in step (f)~~.

34. (Currently amended): A process as claimed in claim 33 wherein the ~~slurry mixture in step (f)~~ is kept at elevated temperature for a period of between 1 minute and 60 minutes.

35. (Currently amended): A process as claimed in claim 33 wherein the ~~slurry mixture in step (f)~~ is heated at a heating rate of between 2 °C per minute and 20 °C per minute.

36. (Canceled)

37. (Previously presented): A process as claimed in claim 1 wherein the citric acid is added to the coal-containing fraction as a citric acid solution containing between 5% and 20% by weight citric acid (hydrated basis).

38. (Currently amended): A process as claimed in claim 37 wherein the ~~slurry mixture in step (f)~~ is heated to a temperature of between 240 °C to 280 °C.

39. (Currently amended): A process as claimed in claim 37 wherein the ~~slurry~~
mixture in step (f) is heated to a temperature of between 150 °C and 160 °C.

40. (Canceled)

41. (Currently amended): A process as claimed in claim 38 wherein the ~~slurry~~
mixture in step (f) is at elevated temperature for a period of between 1 minutes and 60 minutes.

42. (Currently amended): A process as claimed in claim 38 wherein the ~~slurry~~
mixture in step (f) is heated to the elevated temperature at a heating rate of between 2 °C per
minute and 20 °C per minute.

43. (Currently amended): A process as claimed in claim 1 wherein the coal
containing portion ~~recovered~~ from step (g) is washed with water.

44. (Currently amended): A process as claimed in claim 1 wherein ~~demineralised~~
the coal containing portion ~~recovered~~ from step (g) has an ash content of from 0.01-0.2%, by
weight.

45. (Canceled)

46. (Canceled)

47. (Canceled)

48. (Previously presented): A process as claimed in claim 1 wherein the spent
alkali leachant from step (c) is treated to regenerate caustic and to recover minerals.

49. (Original): A process as claimed in claim 48 wherein the spent alkali
leachant is treated by mixing with one or more of calcium oxide, calcium hydroxide, magnesium
oxide, magnesium hydroxide, or mixed oxides or hydroxide of calcium and magnesium derived

from dolomite to precipitate soluble silicate and aluminate ions and from soluble sodium hydroxide.

50. (Previously presented): A process as claimed in claim 1 wherein the substantially liquid fraction of step (e) is treated to regenerate a caustic solution and to recover minerals.

51. (Original): A process as claimed in claim 50 wherein the substantially liquid fraction is mixed with one or more of calcium oxide, calcium hydroxide, magnesium oxide, magnesium hydroxide, or mixed oxides or hydroxide of calcium and magnesium derived from dolomite.